

**Quiz 10**  
**Chemical Engineering Thermodynamics**  
**March 23, 2017**

Determine the fugacity (MPa) for ethane at (a) 7°C (280°K) and 1 MPa and (b) 7°C (280°K) and 4.0 MPa using the virial equation and the shortcut vapor pressure.

$$T_c = 305.3 \text{ °K}, P_c = 4.9 \text{ MPa}, V_c = 147 \text{ cm}^3/\text{mole}, \omega = 0.099, R = 8.314 \text{ J}/(\text{mole °K}) = 8.314 \text{ cm}^3\text{MPa}/(\text{mole°K})$$

Determine if the short cut method is appropriate.

Calculate the vapor pressure and determine the state for each condition.

Determine if the virial equation is appropriate. (*Accept if you are within 10% of the criterion*)

Calculate the fugacity (using different methods for the different states).

$$\log_{10} P_r^{sat} = \frac{7}{3}(1 + \omega)\left(1 - \frac{1}{T_r}\right)$$

9.11

 Shortcut vapor pressure equation. Use care with the shortcut equation below  $T_r = 0.5$ .

$$\ln \varphi = \frac{BP}{RT}$$

9.31

$$Z = 1 + (B^0 + \omega B^1)P_r/T_r \quad \text{or} \quad Z = 1 + BP/RT \quad 7.6$$

$$\text{where } B(T) = (B^0 + \omega B^1)RT_c/P_c \quad 7.7$$

$$B^0 = 0.083 - 0.422/T_r^{1.6} \quad 7.8$$

$$B^1 = 0.139 - 0.172/T_r^{4.2} \quad 7.9$$

$$\text{Subject to } T_r > 0.686 + 0.439P_r \text{ or } V_r > 2.0 \quad 7.10$$

 Poynting correction.

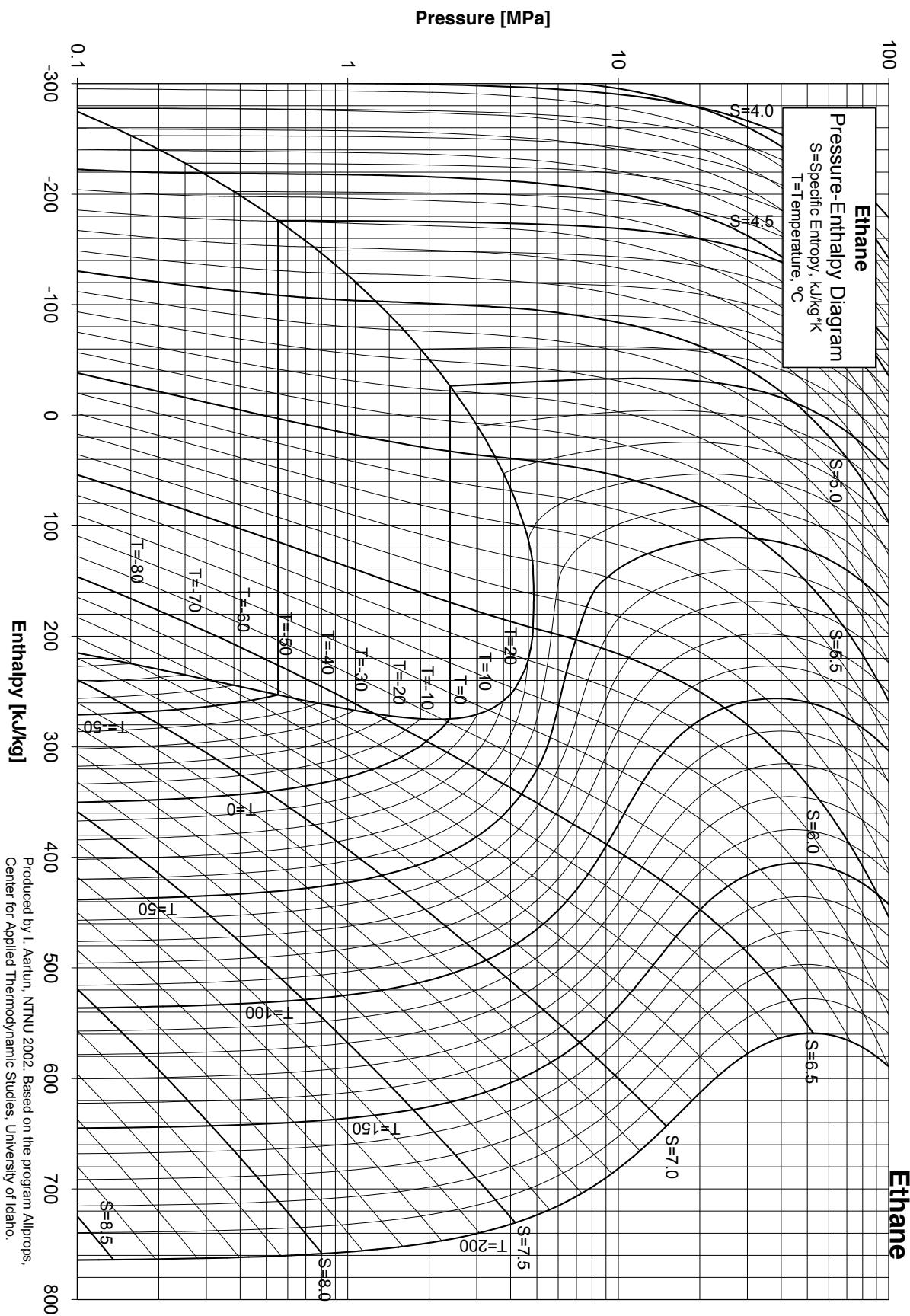
The fugacity is then calculated by

$$f = \varphi^{sat} P^{sat} \exp\left(\frac{V^L(P - P^{sat})}{RT}\right)$$

9.39

Saturated liquid volume can be estimated within a slight percent error using the **Rackett** equation

$$V^{satL} = V_c Z_c^{(1 - T_r)^{0.2857}} \quad 9.40$$
$$Z_c = P_c V_c / (R T_c)$$



Answers Qn. 7 10  
CHC Theme  
March 23, 2017

(a)  $T_r = \frac{280\text{K}}{307\text{K}} = 0.918$

$$P_r = \frac{1.0 \text{ MPa}}{4.9 \text{ MPa}} = 0.204$$

(-3) (1)  
If calc.  
 $T_r$  half dut  
shot

$T_r > 0.5$  so startat walls

$$P_{sat} = P_c 10^{7/3((1-w)(1-\frac{1}{T_r}))}$$

$$= 4.9 \text{ MPa } 10^{7/3(1.099)(1-\frac{1}{0.918})}$$

(2)  $P_{sat} = 2.89 \text{ MPa}$

(3) (1) MPa (Vapor)

(-8) wrong

$$0.686 + 0.439(0.204) = 0.776 \approx 0.918$$

so (V)ant is appropriate

M. say - 5

$$\beta_0 = 0.083 - 0.422 \frac{T_r^{1.6}}{T_r^{4.2}} = -0.407$$

$$\beta_1 = 0.139 - 0.172 \frac{T_r^{4.2}}{T_r^{1.6}} = -0.107$$

$$\beta = (\beta_0 + w\beta_1) \frac{RT_c}{P_c} = -213 \frac{\text{cm}^3}{\text{mole}}$$

①

②

$$\psi = \exp \left( \frac{-213 \frac{\text{cm}^3}{\text{mole}} \frac{1 \text{MPa}}{280}}{8.31 \frac{\text{J/K}}{\text{mole}}} \right)$$

$$\approx 0.913$$

⑤

$$f = 0.913 \text{ MPa}$$

⑥

$$P_{\text{sat}} = 2.89 \text{ MPa} \quad P_r^{\text{sat}} = 0.590$$

$$① P = 4 \text{ MPa} \quad \text{so } L_{\text{liquid}} \quad P_r = \frac{4 \text{ MPa}}{2.89 \text{ MPa}} = 0.816 \quad \text{(-5)}$$

Test for uniaxial using  $P_{\text{sat}}$

②

$$0.686 + 0.439(0.590) = 0.945 \sim T_r = 0.918$$

within 10%

min (-5)

③

$$\ln \phi^{\text{rat}} = \frac{\beta P^{\text{rat}}}{RT} = -\frac{213 \frac{\text{cm}^3}{\text{mole}} 2.89 \text{ MPa}}{8.31 \frac{\text{J/K}}{\text{mole}} 280 \text{ K}} = -0.265$$

$$\phi^{\text{rat}} = 0.767$$

 $P_{\text{sat}}$  (-5)

$$f^{\text{rat}} = \phi^{\text{rat}} P^{\text{rat}} = (0.767) 2.89 \text{ MPa}$$

(-5) or  
problem part

$$f^{\text{rat}} = 2.22 \text{ MPa}$$

④

$$\begin{aligned} V^{\text{rat}} &= 147 \frac{\text{cm}^3}{\text{mole}} \left( \frac{P_0 V_0}{R T_c} \right)^{(1-T_r)^{0.2657}} \\ &= 147 \frac{\text{cm}^3}{\text{mole}} (0.284)^{0.489} = 120 \frac{\text{cm}^3}{\text{mole}} \end{aligned}$$

79.3  $\frac{\text{cm}^3}{\text{mole}}$

(3)

$$f = (0.767)(2.89 \text{ MPa}) \exp\left(\frac{\frac{79.3}{72.0} \frac{m^3}{\text{mole}} (T - 298)}{\frac{0.01}{280} \frac{m^3 \text{ K}}{\text{mole}}}\right)$$

(5)

$$\boxed{f = 23.5 \text{ MPa}}$$

2.30